

PIPENET - Suter Curve for Turbo Pump

How to Estimate Suter Curve from Pump Performance Curve

1. Introduction

Typically, it is possible to obtain the performance curve for the pump in the positive quadrant without difficulty. In this quadrant both the flowrate and the head are positive. However, in order to model the behaviour of a pump in certain situations it is necessary to consider all four quadrants. In other words, both positive and negative values for the head and the flowrate need to be considered. However, this kind of data is often extremely difficult to obtain and even pump manufacturers do not generally have such data.

The classic text book called Fluid Transients by Wylie and Streeter outlines a technique based on the use of Suter Curves for modelling the behaviour of a pump in all four quadrants. It also gives the Suter Curves for a limited range of pumps. Nevertheless, unless pump data is available for all four quadrants, it is not possible to determine the Suter Curves for other pumps accurately.

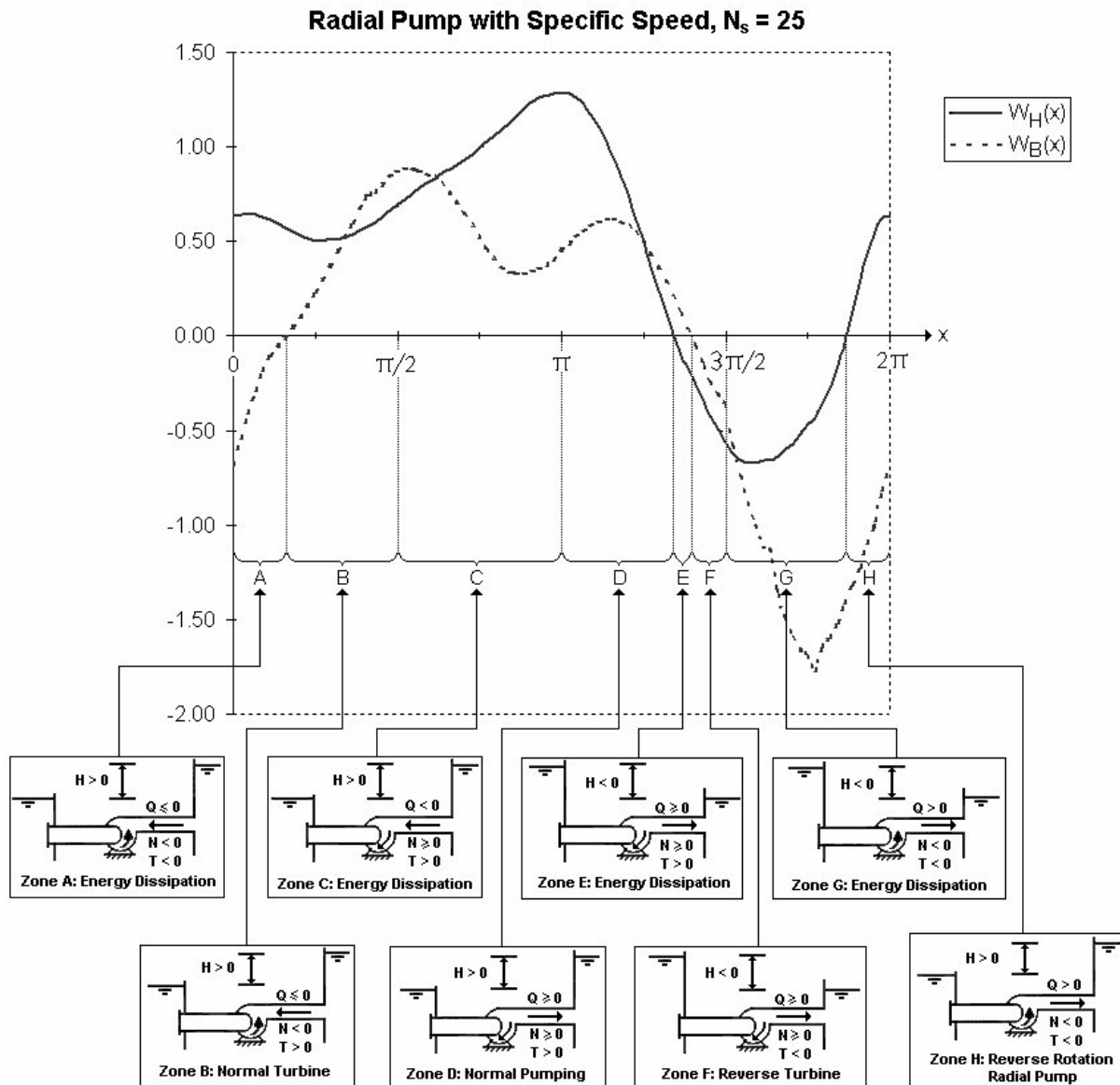
In this document we show how to use the PIPENET built-in Suter Curves and the known pump performance curve (in the positive quadrant) to achieve the following:

- a. In the positive quadrant where the pump curve is known, the Suter Curve follows the pump curve
- b. In the other three quadrants where the pump behaviour is not known we extrapolate the built-in curves

2. Background

During transient flow, a pump may experience a reversal in flow through the pump, or a change in its rotational speed, or both. Furthermore, it may also experience negative torque values and/or pressures during a transient event. Hence for accurate simulation of a Turbo pump, more performance data is needed and this should cover regions of abnormal operation. Suter curve graphically represents all operating status of turbo pump. A detailed description of the Suter Curve and the corresponding concepts and equations refers to the web site of Sunrise Systems Limited and the Transient Module Technical Manual, Chapter 1 – Modelling Aspects, page 16-19.

The figure shows typical Suter curves for a Radial Pump. A whole Suter curve should cover all four Quadrants, i.e. $0-2\pi$ phase angle. There are eight possible zones of pump operation: four occur during normal operation and four are abnormal zones. During a transient event, a pump may enter most, if not all, regions in the figure depending on the appropriate circumstances. However, not all manufactories can provide whole range Suter curves. In most cases only the information at the normal operating condition can be obtained, i.e. Zone D in the above figure. Now the key question is “Is it possible to deduce a whole range Suter curve reasonably in this case?” This document introduces a simple way to solve this problem.

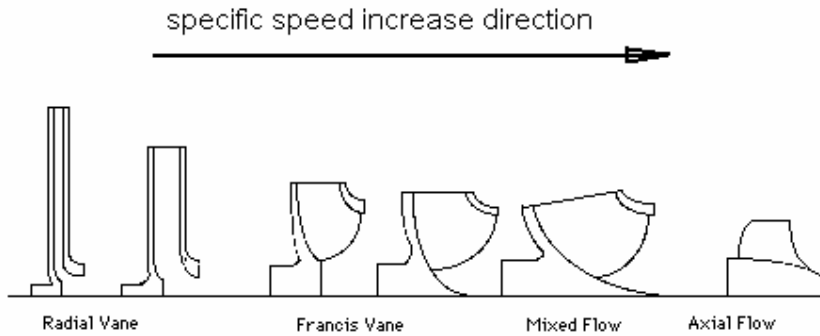


3. Methodology

It is well known that Pumps are traditionally divided into three types: radial pump, mixed pump and axial pump. The classification is tightly relative with specific speed (N_s), see the equation and the figure below:

$$N_s = \frac{N_R \sqrt{Q_R}}{H_R^{0.75}} \quad (1)$$

- N_s : specific speed
- N_R : rated pump speed, rpm
- Q_R : rated pump flowrate, m^3/s
- H_R : rated pump piezometric head, m



Three built-in Suter curves represent three typical pumps: (1) Radial Pump @ $N_s=25$, (2) Mixed Pump @ $N_s=147$ and (3) Axial Pump @ $N_s=261$. Please notice their units when using the above equation to calculate specific speed. In order to supply the lack part of Suter curve for a certain pump, we must base on these three built-in Suter curves and make some assumptions.

- Assumption 1: a specific speed is only mapped to a pump type and the value shift from radial pump to axial pump is continual and uninterrupted.
- Assumption 2: a Suter curve is only match with a pump type and the shift from radial pump to axial pump is continual and uninterrupted.
- Assumption 3: any Suter curve between the two built-in Suter curves has a linear relationship with the specific speeds.

In the next section, we will show the method by an instance.

4. Example 1 – Deduce Suter Curve from a known P-Q curve

In this section we should how to derive the Suter Curve from the known performance curve in the positive quadrant. We also show that the Suter Curve derived in this manner follows the performance curve of the pump faithfully. The last table in this section compares the performance curve which we input and the results obtained from the corresponding Suter Curve.

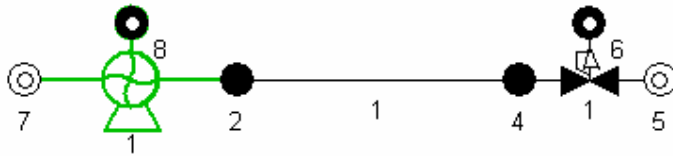
- The known parameters:
 $H_R = 47.5 \text{ m}$
 $Q_R = 42840 \text{ m}^3/\text{hr}$
 $N_R = 6.16667 \text{ 1/s} = 370 \text{ rpm}$
 $T_R = 164 \text{ KN.m}$
 $I = 11530 \text{ kg.m}^2$

Turbo Pump Characteristic and Suter Curve

Q_R	Q	v	H_R	H	h	N_R	α	η	P	T_R	T	β	α^2+v^2	W_H	W_B	x
m^3/h			m			rpm		%	KW	KN.m						
42840	0.00	0.00	47.50	79.50	1.67	370	1.00	0.0%	5007	164.0	129.2	0.79	1.00	1.67	0.79	3.14
42840	5000	0.12	47.50	75.20	1.58	370	1.00	20.5%	5126	164.0	132.3	0.81	1.01	1.56	0.80	3.26
42840	10000	0.23	47.50	71.1	1.50	370	1.00	38.0%	5229	164.0	135.0	0.82	1.05	1.42	0.78	3.37
42840	15000	0.35	47.50	66.6	1.40	370	1.00	51.0%	5475	164.0	141.3	0.86	1.12	1.25	0.77	3.48
42840	20000	0.47	47.50	61.7	1.30	370	1.00	62.0%	5563	164.0	143.6	0.88	1.22	1.07	0.72	3.58
42840	25000	0.58	47.50	58.2	1.23	370	1.00	71.0%	5728	164.0	147.8	0.90	1.34	0.91	0.67	3.67
42840	30000	0.70	47.50	56	1.18	370	1.00	79.0%	5944	164.0	153.4	0.94	1.49	0.79	0.63	3.75
42840	35000	0.82	47.50	54.3	1.14	370	1.00	85.4%	6220	164.0	160.5	0.98	1.67	0.69	0.59	3.83
42840	40000	0.93	47.50	50.8	1.07	370	1.00	89.1%	6374	164.0	164.5	1.00	1.87	0.57	0.54	3.89
42840	42840	1.00	47.50	47.5	1.00	370	1.00	89.5%	6355	164.0	164.0	1.00	2.00	0.50	0.50	3.93
42840	45000	1.05	47.50	44.6	0.94	370	1.00	88.6%	6331	164.0	163.4	1.00	2.10	0.45	0.47	3.95
42840	50400	1.18	47.50	37	0.78	370	1.00	82.8%	6295	164.0	162.5	0.99	2.38	0.33	0.42	4.01

- Scenario:

The test-bed for checking that the Suter Curve follows the pump performance curve in the positive quadrant is described here. (This pump performance curve is normally provided by the pump manufacturer.)



Pump types (Turbo)

Description: Turbo Pump

Rated Quantities

Pressure (m fluid)	47.5	Flowrate (m³/hr)	42840
Speed (1/secs)	6.16666667	Torque (N.m)	164004

Moment of Inertia (kg.m²) 11530

Curve Data: User Defined

x	WH(x)
3.14	1.67
3.26	1.56
3.37	1.42
3.48	1.25
3.58	1.07
3.67	0.91
3.75	0.79

x	WB(x)
3.14	0.79
3.26	0.8
3.37	0.78
3.48	0.77
3.58	0.72
3.67	0.67
3.75	0.63

Library Information

Filed Turbo Pump.PLB

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- Results:

In this section we show that the results from the test-bed follow the actual pump curve which was used to generate the Suter Curve.

We change the flowrate specification at the node 5 to check the relationship of the flow rate and pressure lift of the turbo pump. We can see the input data roughly equal to the calculated results, see the table below.

Flow Rate	m ³ /h	0.00	5000	10000	15000	20000	25000	30000	35000	40000	42840	45000	50400
Input Lift	m	79.5	75.2	71.1	66.6	61.7	58.2	56.0	54.3	50.8	47.5	44.6	37.0
Calculated Lift	m	79.26	75.21	71.06	66.79	62.07	57.97	55.71	54.99	50.26	48	44.65	37.85
Error	%	-0.3%	0.0%	-0.1%	0.3%	0.6%	-0.4%	-0.5%	1.3%	-1.1%	1.1%	0.1%	2.3%

5. Example 2 - Deduce unknown Suter Curve from the known part

In this section we show how to extrapolate the built-in Suter Curves to the cases where the Suter Curve is not known. It is important to emphasise that this technique of extrapolating known data to unknown data, and it should be regarded as an approximation.

- The known parameters:
 $H_R = 47.5 \text{ m}$
 $Q_R = 42840 \text{ m}^3/\text{hr}$
 $N_R = 6.16667 \text{ 1/s} = 370 \text{ rpm}$
 $T_R = 164 \text{ KN.m}$
 $I = 11530 \text{ kg.m}^2$

The known part of Suter curve

X	3.14	3.26	3.37	3.48	3.58	3.67	3.75	3.83	3.89	3.93	3.95	4.01
Wh	1.67	1.56	1.42	1.25	1.07	0.91	0.79	0.69	0.57	0.50	0.45	0.33
W _B	0.79	0.80	0.78	0.77	0.74	0.67	0.63	0.59	0.54	0.50	0.47	0.42

- The pseudo specific speeds at the boundaries:
 The real specific speed can be calculated by Equation 1, see the table below. The calculated pump ($N_s=70.54$) is between radial pump ($N_s=25$) and mixed pump ($N_s=147$). Therefore, the deduced Suter curve will be based on the data for these two built-in Suter curves.

Name	Symbol	Value	Unit
Rated pump speed	N_R	370	rpm
Rated pump flowrate	Q_R	11.90	m ³ /s
Rated pump piezometric head	H_R	47.5	m
Specific speed	N_s	70.54	

From the known Suter curve, we can interpolate to obtain the pseudo specific speeds at the boundaries ($X=3.14$ and $X=4.01$), see the table below:

Boundaries	X	3.14	4.01
Built-in radial pump	Wh	1.288	0.35
	W _B	0.45	0.42
	N _s	25	25
Built-in mixed pump	Wh	1.97	0.348
	W _B	1.49	0.389
	N _s	147	147
The calculated pump	Wh	1.67	0.33
	N _s (Wh)	93.33	70.54
	W _B	0.79	0.42
	N _s (W _B)	64.88	70.54

For example, the pseudo specific speed for the head curve (Wh) at the boundary of X=3.14 can be calculated by:

$$N_s = 25 + \frac{1.67 - 1.288}{1.97 - 1.288} \times (147 - 25) = 93.33$$

However, at the boundary of X=4.01, the two built-in head curve is too close to use interpolation simply. Otherwise, it may cause great error. See the calculation below:

$$N_s = 25 + \frac{0.33 - 0.35}{0.348 - 0.35} \times (147 - 25) = 1245$$

The obtained value is ridiculously big. Therefore, we recommend the actual specific speed (70.54) in this case.

Now, we have obtained four pseudo specific speeds at two Suter curves boundaries, i.e. head curve (Wh) and torque curve (W_B). Next step, we will deduce a whole Suter curve for the calculated pump.

- A whole Suter curve:

First, we assume the specific speeds at the unknown zone linearly shift between the two abovementioned boundaries, i.e. phase angle from X=4.01 to X=3.14+2π. Here, 2π means pump curve get into next circle. For instance, the pseudo specific speed for head curve at the phase angle of 0 can be calculated by:

$$N_s = 93.33 + \frac{(0 + 2\pi) - 4.01}{(3.14 + 2\pi) - 4.01} \times (70.54 - 93.33) = 83.76$$

For instance again, the pseudo specific speed for head curve at the phase angle of 1.5π can be calculated by:

$$N_s = 93.33 + \frac{1.5\pi - 4.01}{(3.14 + 2\pi) - 4.01} \times (70.54 - 93.33) = 90.37$$

After getting the pseudo specific speeds at whole range phase angle (except the known zone), we can deduce the unknown part of Suter curve by the interpolated method, the following table show the calculating process at the phase angles of 0 and 1.5π.

Boundaries	X	0	1.5π
Built-in radial pump	Ns	25	25
	Wh	0.634	-0.556
Built-in mixed pump	Ns	147	147
	Wh	-0.69	-1.5
The calculated pump	Ns	83.76	90.37
	Wh	-0.004	-1.062

In detail, for the head curve @ X=0,

$$Wh = 0.634 + (-0.69 - 0.634) \times \frac{83.76 - 25}{147 - 25} = -0.004$$

6. Program

In this section we show how our spreadsheet program can be used for extrapolating the built-in Suter Curve to represent the actual pump.

Although the abovementioned method is not difficult to understand, the actual calculation is very enormous. Of course, this simple and repeated work can be done easily by computer. Therefore, a small program was written in Excel. The whole range Suter curve can be obtained just by inputting the boundaries conditions, i.e. the phase angles and the pseudo specific speeds at the start and end points of the known zone. However, the input pseudo specific speeds must be between 25 and 261 because the unacceptable error may be caused by external interpolation. The table below exhibits the calculated results for the above example. All needed input data is coloured in red and all known part of Suter curve is marked as “-“ respectively.

7. Summary

The steps to approach Suter curve are:

- (1). Obtain the relative information from the manufactory, which include P-Q curve, pump speed curve, efficiency curve (or power curve), rated flow rate, head, speed and the total moment of inertia of the pump.
- (2). Calculate the known part of Suter curve.
- (3). Deduce the specific speed of the pump.
- (4). Interpolate the pseudo specific speed at the ends of the known Suter curve.
- (5). Input the deduced data, i.e. the pseudo specific speed and the corresponding phase angle, into the Excel program to get entire range Suter curve.

No.	Built-in Standard Suter Curve				Deduced Suter Curve			
	Phase Angle	Head Curve (Wh)			Input Data		Output Data	
		X	Ns=25	Ns=147	Ns=261	Start Point	Ns	Wh
0	0.0000	0.634	-0.690	-2.230	X	3.140	79.827	0.039
1	0.0714	0.643	-0.599	-2.000	Wh	1.67	80.089	0.082
2	0.1428	0.646	-0.512	-1.662	Ns	91.3	80.350	0.121
3	0.2142	0.640	-0.418	-1.314	End Point		80.612	0.158
4	0.2856	0.629	-0.304	-1.089	X	4.010	80.874	0.202
5	0.3570	0.613	-0.181	-0.914	Wh	0.330	81.135	0.248
6	0.4284	0.595	-0.078	-0.760	Ns	71.500	81.397	0.284
7	0.4998	0.575	-0.011	-0.601			81.658	0.303
8	0.5712	0.552	0.032	-0.440			81.920	0.309
9	0.6426	0.533	0.074	-0.284			82.181	0.318
10	0.7140	0.516	0.130	-0.130			82.443	0.334
11	0.7854	0.505	0.190	0.065			82.704	0.356
12	0.8568	0.504	0.265	0.222			82.966	0.390
13	0.9282	0.510	0.363	0.357			83.228	0.440
14	0.9996	0.512	0.461	0.493			83.489	0.488
15	1.0710	0.522	0.553	0.616			83.751	0.537
16	1.1424	0.539	0.674	0.675			84.012	0.604
17	1.2138	0.559	0.848	0.680			84.274	0.699
18	1.2852	0.580	1.075	0.691			84.535	0.822
19	1.3566	0.601	1.337	0.752			84.797	0.962
20	1.4280	0.630	1.629	0.825			85.058	1.122
21	1.4994	0.662	1.929	0.930			85.320	1.288
22	1.5708	0.692	2.180	1.080			85.582	1.431
23	1.6422	0.722	2.334	1.236			85.843	1.526
24	1.7136	0.753	2.518	1.389			86.105	1.637
25	1.7850	0.782	2.726	1.548			86.366	1.760
26	1.8564	0.808	2.863	1.727			86.628	1.846
27	1.9278	0.832	2.948	1.919			86.889	1.905
28	1.9992	0.857	3.026	2.066			87.151	1.962
29	2.0706	0.879	3.015	2.252			87.412	1.972
30	2.1420	0.904	2.927	2.490			87.674	1.943
31	2.2134	0.930	2.873	2.727			87.936	1.932
32	2.2848	0.959	2.771	3.002			88.197	1.898
33	2.3562	0.996	2.640	3.225			88.459	1.851
34	2.4276	1.027	2.497	3.355			88.720	1.795
35	2.4990	1.060	2.441	3.475			88.982	1.784
36	2.5704	1.090	2.378	3.562			89.243	1.768
37	2.6418	1.124	2.336	3.604			89.505	1.765
38	2.7132	1.165	2.288	3.582			89.766	1.761
39	2.7846	1.204	2.209	3.510			90.028	1.740
40	2.8560	1.238	2.162	3.477			90.290	1.732
41	2.9274	1.258	2.140	3.321			90.551	1.732
42	2.9988	1.271	2.109	3.148			90.813	1.723
43	3.0702	1.282	2.054	2.962			91.074	1.700
44	3.1416	1.288	1.970	2.750			-	-
45	3.2130	1.281	1.860	2.542			-	-
46	3.2844	1.260	1.735	2.354			-	-
47	3.3558	1.225	1.571	2.149			-	-
48	3.4272	1.172	1.357	1.909			-	-
49	3.4986	1.107	1.157	1.702			-	-
50	3.5700	1.031	1.106	1.506			-	-
51	3.6414	0.942	0.927	1.310			-	-
52	3.7128	0.842	0.846	1.131			-	-
53	3.7842	0.733	0.744	0.947			-	-
54	3.8556	0.617	0.640	0.737			-	-
55	3.9270	0.500	0.500	0.500			-	-
56	3.9984	0.368	0.374	0.279			-	-
57	4.0698	0.240	0.191	0.082			71.719	0.221
58	4.1412	0.125	0.001	-0.112			71.981	0.077
59	4.2126	0.011	-0.190	-0.300			72.242	-0.067
60	4.2840	-0.102	-0.384	-0.505			72.504	-0.212
61	4.3554	-0.168	-0.585	-0.672			72.765	-0.331
62	4.4268	-0.255	-0.786	-0.797			73.027	-0.464
63	4.4982	-0.342	-0.972	-0.872			73.288	-0.591
64	4.5696	-0.423	-1.185	-0.920			73.550	-0.726
65	4.6410	-0.494	-1.372	-0.949			73.811	-0.845
66	4.7124	-0.556	-1.500	-0.960			74.073	-0.936
67	4.7838	-0.620	-1.940	-1.080			74.335	-1.154
68	4.8552	-0.655	-2.160	-1.300			74.596	-1.267
69	4.9266	-0.670	-2.290	-1.500			74.858	-1.332
70	4.9980	-0.670	-2.350	-1.700			75.119	-1.360
71	5.0694	-0.660	-2.350	-1.890			75.381	-1.358
72	5.1408	-0.655	-2.230	-2.080			75.642	-1.309
73	5.2122	-0.640	-2.200	-2.270			75.904	-1.291
74	5.2836	-0.600	-2.130	-2.470			76.166	-1.242
75	5.3550	-0.570	-2.050	-2.650			76.427	-1.194
76	5.4264	-0.520	-1.970	-2.810			76.689	-1.134
77	5.4978	-0.470	-1.895	-2.950			76.950	-1.077
78	5.5692	-0.430	-1.810	-3.040			77.212	-1.021
79	5.6406	-0.360	-1.730	-3.100			77.473	-0.949
80	5.7120	-0.275	-1.600	-3.150			77.735	-0.848
81	5.7834	-0.160	-1.420	-3.170			77.996	-0.707
82	5.8548	-0.040	-1.130	-3.170			78.258	-0.516
83	5.9262	0.130	-0.950	-3.130			78.520	-0.344
84	5.9976	0.295	-0.930	-3.070			78.781	-0.245
85	6.0690	0.430	-0.950	-2.960			79.043	-0.181
86	6.1404	0.550	-1.000	-2.820			79.304	-0.140
87	6.2118	0.620	-0.920	-2.590			79.566	-0.069
88	6.2832	0.634	-0.690	-2.230			79.827	0.039

No.	Built-in Suter Curve				Deduced Suter Curve			
	Phase Angle	Torque Curve (W _g)			Input Data		Output Data	
		X	Ns=25	Ns=147	Ns=261	Start Point	Ns	W _g
0	0.0000	-0.684	-1.420	-2.260	X	3.140	68.720	-0.948
1	0.0714	-0.547	-1.328	-2.061	W _g	0.79	68.633	-0.826
2	0.1428	-0.414	-1.211	-1.772	Ns	64.9	68.545	-0.698
3	0.2142	-0.292	-1.056	-1.465	End Point		68.458	-0.564
4	0.2856	-0.187	-0.870	-1.253	X	4.010	68.371	-0.430
5	0.3570	-0.105	-0.677	-1.088	W _g	0.420	68.263	-0.308
6	0.4284	-0.053	-0.573	-0.921	Ns	71.500	68.196	-0.237
7	0.4998	-0.012	-0.518	-0.789			68.109	-0.191
8	0.5712	0.042	-0.380	-0.632			68.021	-0.107
9	0.6426	0.097	-0.232	-0.457			67.934	-0.019
10	0.7140	0.156	-0.160	-0.300			67.847	0.045
11	0.7854	0.227	0.000	-0.075			67.760	0.147
12	0.8568	0.300	0.118	0.052			67.672	0.236
13	0.9282	0.371	0.308	0.234			67.585	0.349
14	0.9996	0.444	0.442	0.425			67.498	0.443
15	1.0710	0.522	0.574	0.558			67.410	0.540
16	1.1424	0.596	0.739	0.630			67.323	0.646
17	1.2138	0.672	0.929	0.621			67.236	0.761
18	1.2852	0.738	1.147	0.546			67.148	0.879
19	1.3566	0.763	1.370	0.525			67.061	0.972
20	1.4280	0.797	1.599	0.488			66.974	1.073
21	1.4994	0.837	1.839	0.512			66.886	1.181
22	1.5708	0.865	2.080	0.660			66.799	1.281
23	1.6422	0.883	2.300	0.850			66.712	1.367
24	1.7136	0.886	2.480	1.014			66.624	1.430
25	1.7850	0.877	2.630	1.162			66.537	1.474
26	1.8564	0.859	2.724	1.334			66.450	1.493
27	1.9278	0.838	2.687	1.512			66.362	1.465
28	1.9992	0.804	2.715	1.683			66.275	1.451
29	2.0706	0.758	2.688	1.886			66.188	1.410
30	2.1420	0.703	2.555	2.105			66.101	1.327
31	2.2134	0.645	2.434	2.325			66.013	1.246
32	2.2848	0.583	2.288	2.580			65.926	1.155
33	2.3562	0.520	2.110	2.770			65.839	1.052
34	2.4276	0.454	1.948	2.886			65.751	0.953
35	2.4990	0.408	1.825	2.959			65.664	0.880
36	2.5704	0.370	1.732	2.979			65.577	0.823
37	2.6418	0.343	1.644	2.962			65.489	0.775
38	2.7132	0.331	1.576	2.877			65.402	0.743
39	2.7846	0.329	1.533	2.713			65.315	0.727
40	2.8560	0.338	1.522	2.556			65.227	0.728
41	2.9274	0.354	1.519	2.403			65.140	0.737
42	2.9988	0.372	1.523	2.237			65.053	0.750
43	3.0702	0.405	1.523	2.080			64.965	0.771
44	3.1416	0.450	1.490	1.950			-	-
45	3.2130	0.486	1.386	1.826			-	-
46	3.2844	0.520	1.223	1.681			-	-
47	3.3558	0.552	1.048	1.503			-	-
48	3.4272	0.579	0.909	1.301			-	-
49	3.4986	0.603	0.814	1.115			-	-
50	3.5700	0.616	0.766	0.960			-	-
51	3.6414	0.617	0.734	0.840			-	-
52	3.7128	0.606	0.678	0.750			-	-
53	3.7842	0.582	0.624	0.677			-	-
54	3.8556	0.546	0.570	0.604			-	-
55	3.9270	0.500	0.500	0.500			-	-
56	3.9984	0.432	0.407	0.352			-	-
57	4.0698	0.360	0.278	0.161			71.427	0.329
58	4.1412	0.288	0.146	-0.040			71.340	0.234
59	4.2126	0.214	0.023	-0.225			71.252	0.142
60	4.2840	0.123	-0.175	-0.403			71.165	0.010
61	4.3554	0.037	-0.379	-0.545			71.078	-0.120
62	4.4268	-0.053	-0.585	-0.610			70.990	-0.254
63	4.4982	-0.161	-0.778	-0.662			70.903	-0.393
64	4.5696	-0.248	-1.008	-0.699			70.816	-0.533
65	4.6410	-0.314	-1.277	-0.719			70.728	-0.675
66	4.7124	-0.372	-1.560	-0.730			70.641	-0.816
67	4.7838	-0.580	-2.070	-0.810			70.554	-1.136
68	4.8552	-0.740	-2.480	-1.070			70.466	-1.388
69	4.9266	-0.880	-2.700	-1.360			70.379	-1.557
70	4.9980	-1.000	-2.770	-1.640			70.292	-1.657
71	5.0694	-1.120	-2.800	-1.880			70.204	-1.742
72	5.1408	-1.250	-2.800	-2.080			70.117	-1.823
73	5.2122	-1.370	-2.760	-2.270			70.030	-1.883
74	5.2836	-1.490	-2.710	-2.470			69.942	-1.939
75	5.3550	-1.590	-2.640	-2.650			69.855	-1.976
76	5.4264	-1.660	-2.540	-2.810			69.768	-1.983
77	5.4978	-1.690	-2.440	-2.950			69.681	-1.965
78	5.5692	-1.770	-2.340	-3.040			69.593	-1.978
79	5.6406	-1.650	-2.240	-3.100			69.506	-1.865
80	5.7120	-1.590	-2.120	-3.150			69.419	-1.783
81	5.7834	-1.520	-2.000	-3.170			69.331	-1.694
82	5.8548	-1.420	-1.940	-3.200			69.244	-1.609
83	5.9262	-1.320	-1.900	-3.160			69.157	-1.530
84	5.9976	-1.230	-1.900	-3.090			69.069	-1.472
85	6.0690	-1.100	-1.850	-2.990			68.982	-1.370
86	6.1404	-0.980	-1.750	-2.860			68.895	-1.257
87	6.2118	-0.820	-1.630	-2.660			68.807	-1.111
88	6.2832	-0.684	-1.420	-2.260			68.720	-0.948